

Reply to thread 391-359418

q_G - heat generated by heating element

q_1 - heat transfer thru insulation

q_2 - heat transfer thru adhesive layer & pipe wall

k_i, k_a, k_p : thermal conductivities of insulation, adhesive layer & pipe wall

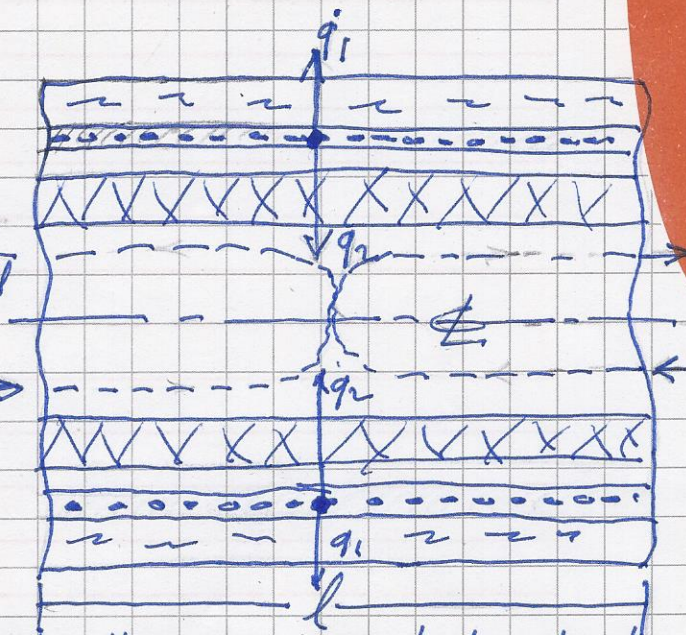
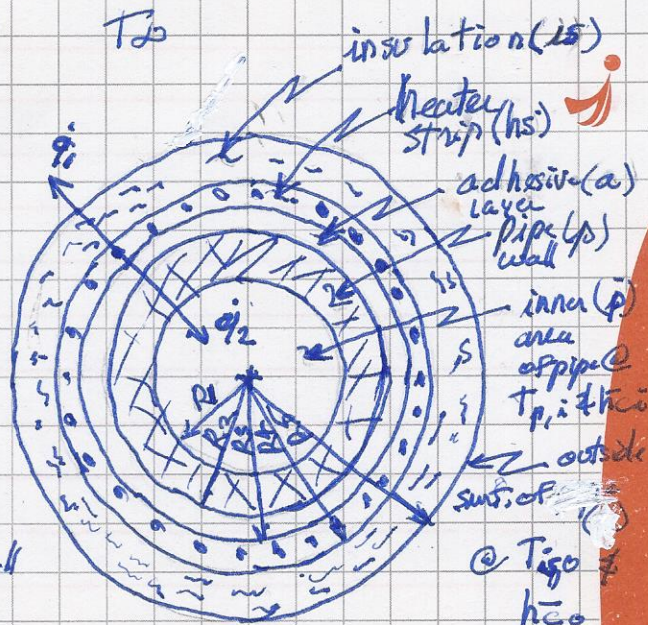
h_{co}, h_{ci} : convective heat transfer coefficient on outside surface of insulation and on the inside surface of pipe wall

$T_{i,o}$ - Temp. of outside surface of insulation

T_b - bulk temperature of air movement inside of pipe.

T_o - ambient temperature

T_h - temperature of heating element



Kent "Power" must estimate $T_{i,o}$

Smith "Heat transfer" graph on Fig 8-2

$Nu \propto Re^{0.3}$
 $Nu \propto .48 Re^{0.3}$

$$h_{co} \approx 0.27 [(T_{i,o} - T_o) / 2 R_i]^{0.25}$$

$$h_{ci} \approx 0.48 (k / 2 R_i) (V D / \mu)^{0.3}$$

Conditions : Steady State; heat flow outwardly & inwardly from heating element
Discard end heat loss; use bulk air temperature (T_b); units in B.T.U.

$$q_G = q_1 + q_2$$

$$q_G = \frac{T_h - T_o}{\frac{\ln(R_5/R_i)}{2\pi k_i l} + \frac{1}{2\pi R_5 h_{co}}} + \frac{T_h - T_b}{\frac{\ln(R_3/R_i)}{2\pi k_a l} + \frac{\ln(R_3/R_i)}{2\pi R_p l} + \frac{1}{2\pi R_i h_{ci}}}$$

Solution is trial & error tempered w/ engineering judgement.

h_{co} & h_{ci} are surface temperature dependent under free air movement (convection).

h_{ci} 's would range between .6 - 5 Btu/hr ft² °F.

known values : $k_i, k_a, k_p; R_i, R_a, R_p, R_5; T_o$

Unknown values : T_b, h_{co}, h_{ci} . We can estimate two reasonable temperature extremes for $T_{i,o}$ & $T_{p,i}$ to calculate two extreme values for h_{co} & h_{ci} and these should interchange much, so average the extreme h_{ci} 's. h_{co} is straight forward but h_{ci} will be determined from $Nu \approx .48 Re^{0.3}$; $Nu = h_{ci} D / k_{air}$ since at T_b $Re = V D / \mu = V D / \nu$ where μ, ν, D are dependent on T_b . Velocity (V) values will be low and must be judged