

Nozzle Loads, Piping Stresses, and the Effect of Piping on Equipment

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November 13, 2009



FLUOR

Topics Covered

- Introduction
- Nozzle Loads – What are they?
- API 610 vs. ANSI Allowable Forces and Moments
- Nozzle Load Issues for Different Pump Types
- Information Stress Engineering Needs
- Special Cases

Please feel free to ask questions!

Introduction

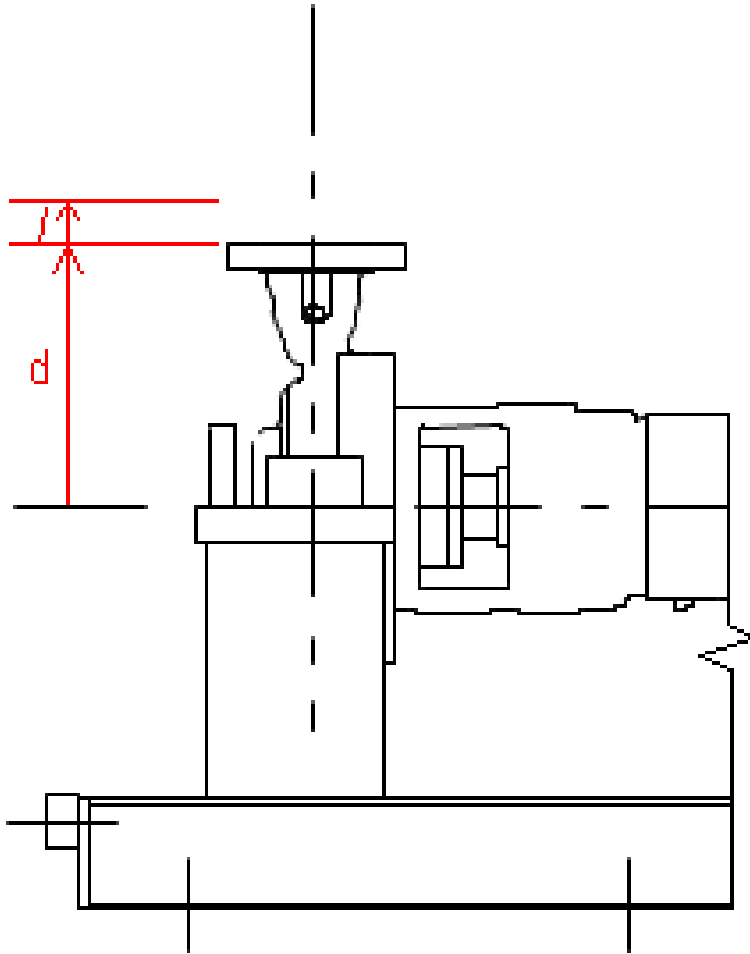
- As Mechanical Equipment Engineers, we need to understand how our equipment interacts with the other aspects of the plant, especially piping.
- All API equipment codes have formulas or tables for “Allowable Nozzle Loads” – but what do they really mean?
- Lets go back to our university statics course for a moment...

What are Nozzle Loads?

- Nozzle loads are the net forces and moments exerted on equipment nozzles from the weight and thermal expansion of connected piping and equipment.
- The loads exerted on equipment are directly related to how the equipment and piping are supported.
- Increased nozzle loads are a cause of misalignment and increased wear and vibration rates in pumps.

What are Equipment Nozzle Loads?

Continued...

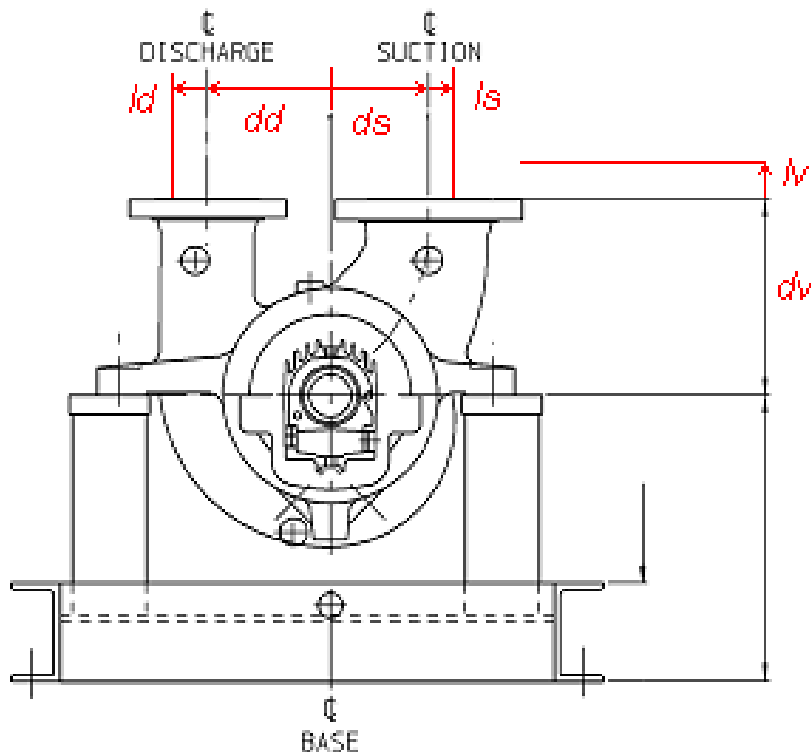


- Thermal Growth
 - l = growth
 - d = centreline to nozzle flange distance
 - α = thermal growth factor
 - (for Carbon Steel @ 100°C $\alpha = 1.1\text{in}/100\text{ft}$)
- On an OH2 pump, the discharge nozzle will grow with temperature, exerting a force on the piping above.

What are Equipment Nozzle Loads?

Continued...

- Between bearing pumps are more complicated because the nozzles thermally grow up from the centreline, as well as horizontally away from the centreline.



- d_v = centreline to top of nozzle
- l_v = vertical nozzle growth
- d_s = centreline to centre of suction nozzle
- l_s = suction nozzle horizontal growth
- d_d = centreline to centre of discharge nozzle
- l_d = discharge nozzle horizontal growth
- Assuming point of zero expansion is the centreline of the shaft

The Piping Effect

- Piping adds another dimension
- The layout and support of the piping will affect the forces and moments exerted on the equipment.
- The net force on the discharge nozzle of a pump is the force of the piping weight and thermal expansion load minus the force of the nozzle's thermal growth.
- “For horizontal pumps, two effects of nozzle loads are considered: Distortion of the pump casing and misalignment of the pump and driver shafts.”

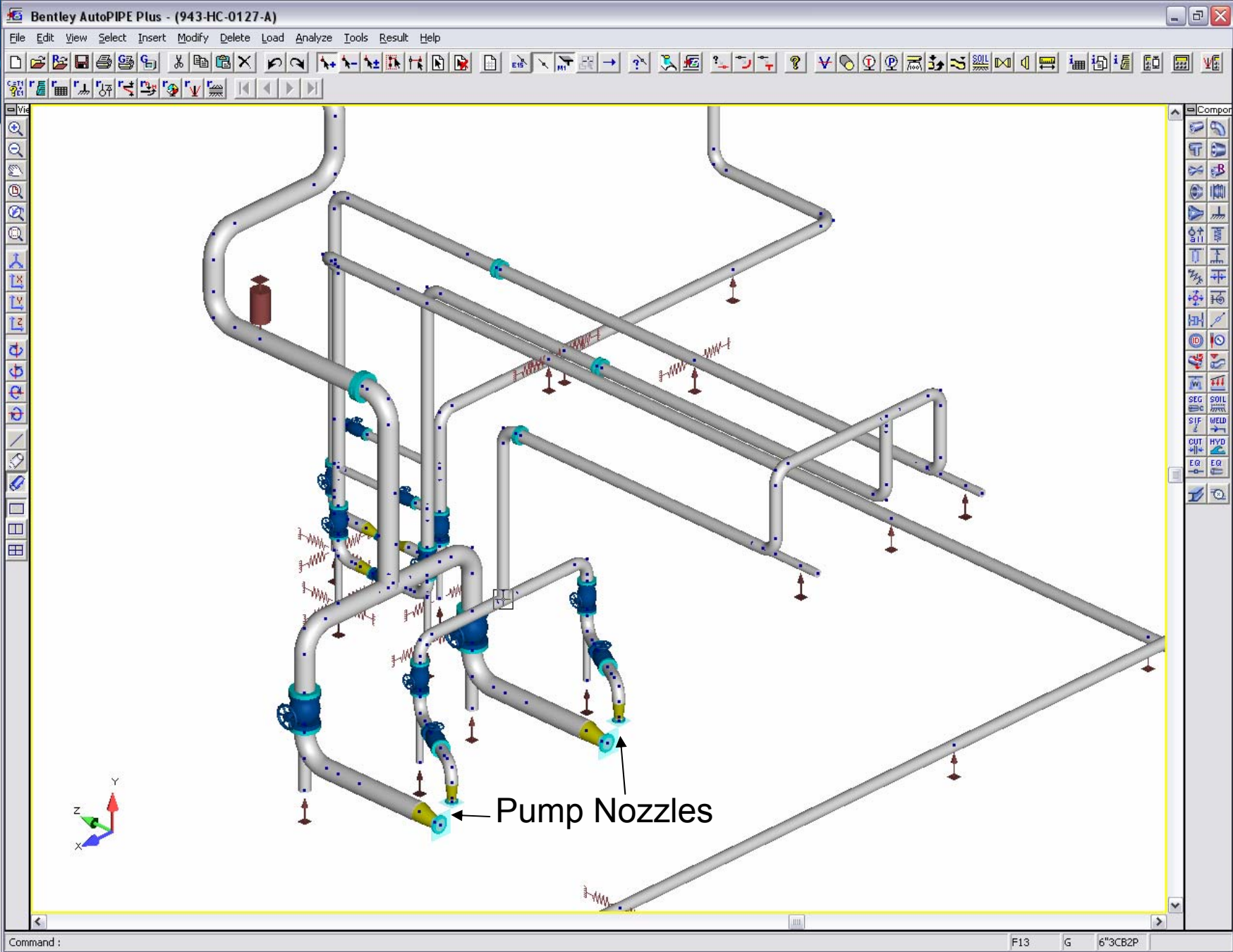
API 610 10th Ed. 5.5.1

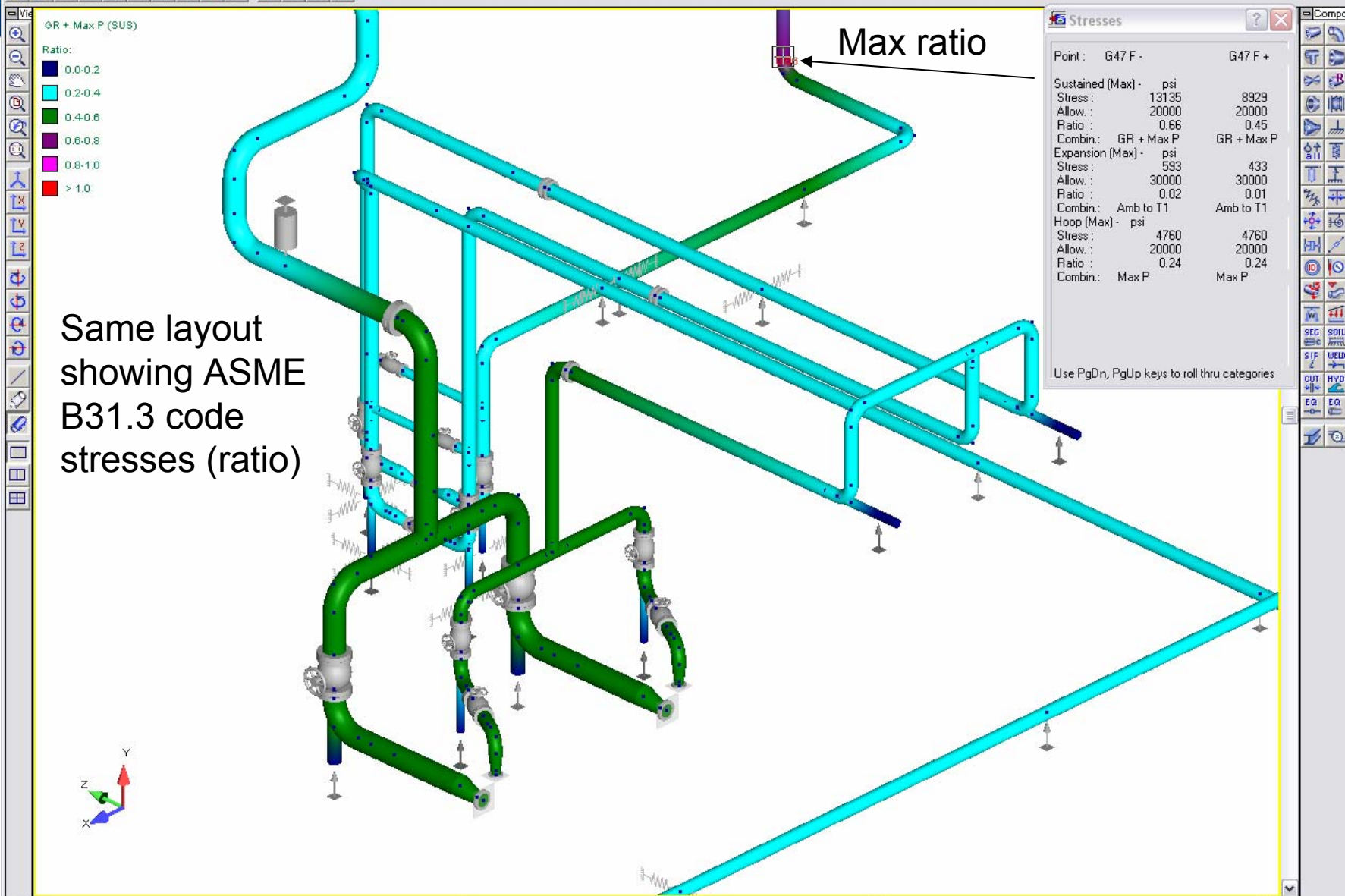
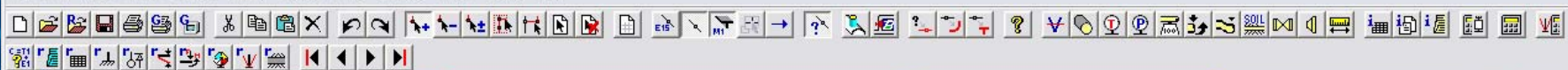
Factors that Affect Nozzle Loads

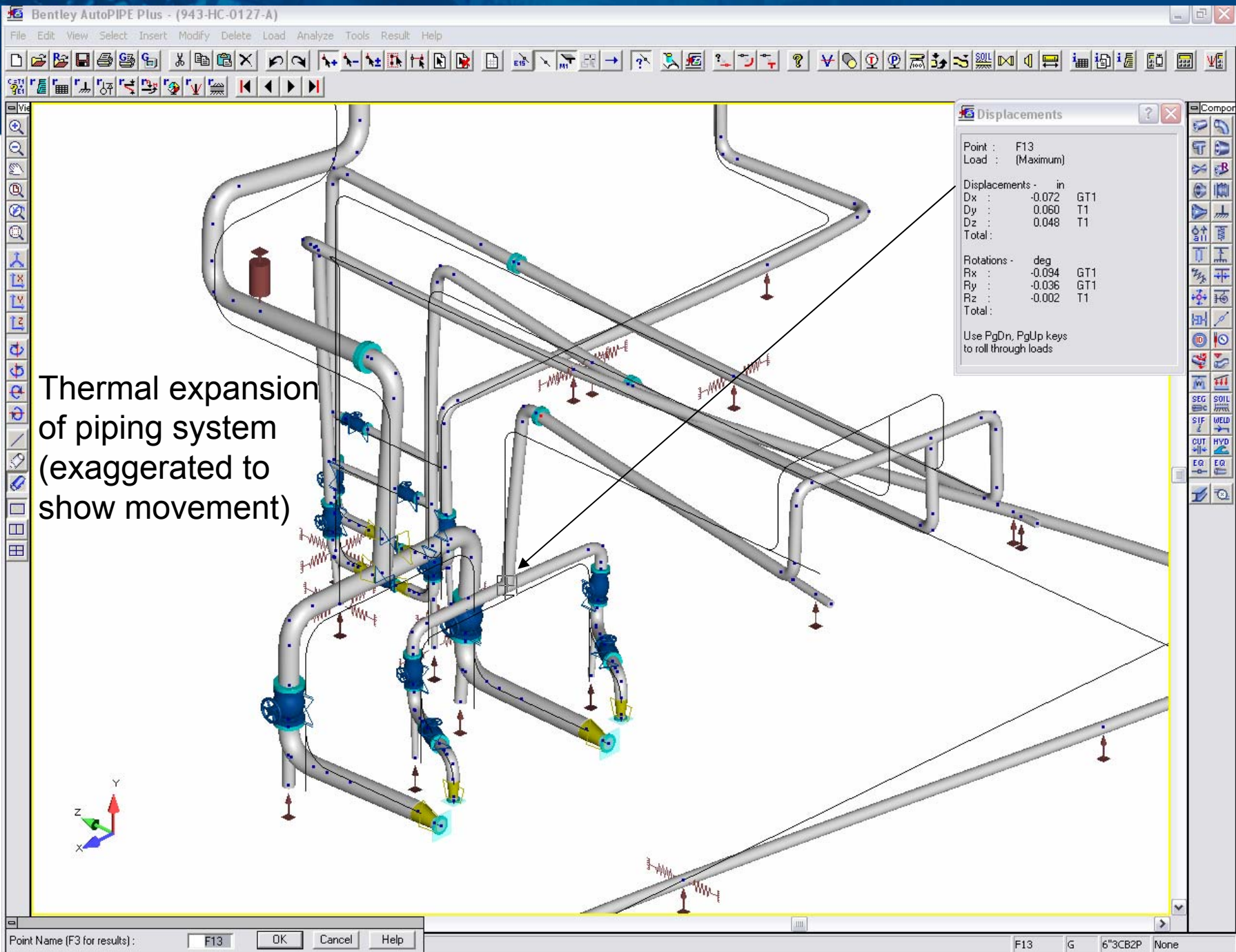
- Temperature
 - Affects expansion of piping/equipment
- Pressure
 - Affects pipe stiffness (more pressure = thicker pipe)
- Client piping layout requirements
 - Valves at grade or overhead
 - Maintenance access
- Steel / Support locations available
- Baseplate design

Stress Engineering Tools

- Stress engineers use specialized FEA software packages to do calculations (AutoPIPE®, CAESAR II)
- Allows engineer to build a 3D model of the piping system, add supports, temperature and pressure information, and see how the piping reacts
- Shows movement of the pipe, stresses on the pipe, and loads on supports and equipment flanges
- AutoPIPE® Break...
 - 6x4 OH2 Pump
 - Flow = 909gpm, Head = 426ft, HP = 150hp

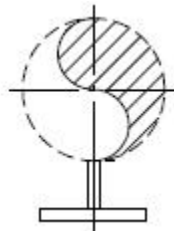
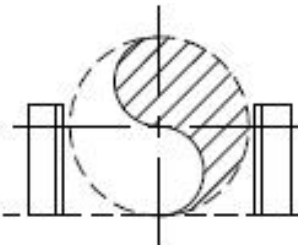
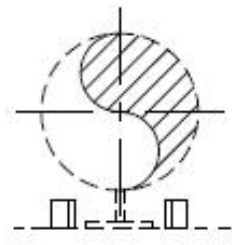
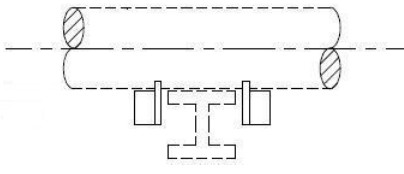
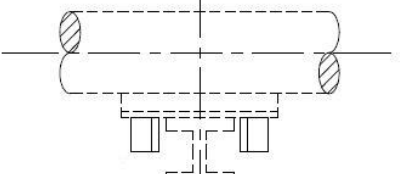






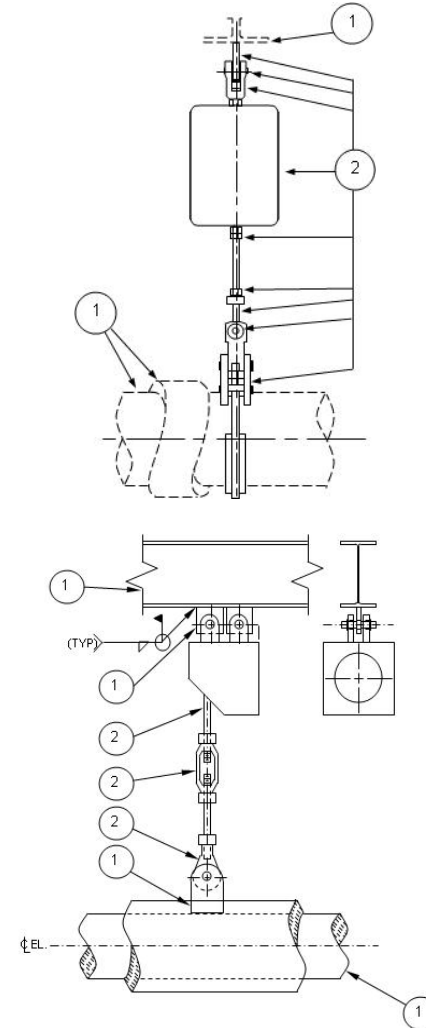
Piping Support Types

- Vertical Support – keeps the pipe from falling down
 - Eg. Support steel, shoe, base support, spring
- Horizontal Guide – holds the pipe parallel to its axis
- Directional Anchor (DA) – holds the pipe perpendicular to its axis; thermal growth will occur in both directions along the pipe axis
- Full Anchor – combination of a guide and directional anchor; pipe will not move in any direction

Typical pipe support details	Shoe 
Guide - no shoe 	Guide - w/ shoe 
Directional Anchor - no shoe 	Directional Anchor - w/ shoe 

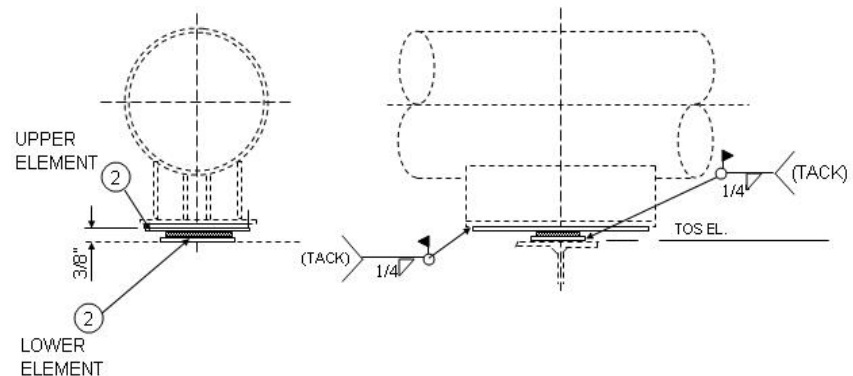
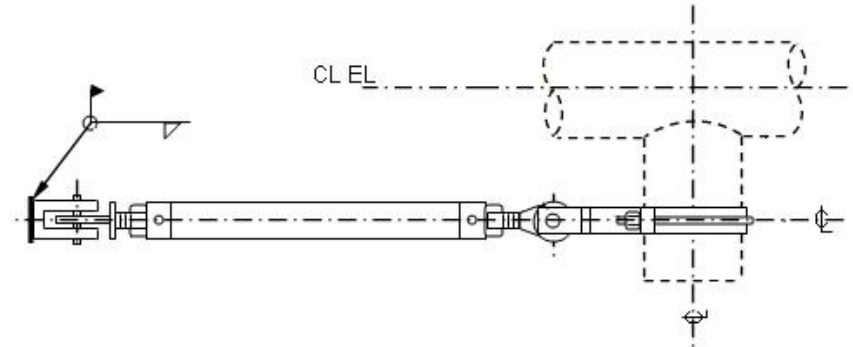
Special Piping Supports

- Variable Spring
 - Takes the weight load (GR) to reduce load in vertical direction
 - Does not impose a reaction load because spring moves up or down
 - As pipe moves, spring reacts
- Constant Spring
 - Similar to variable spring
 - Used for vertical movements > 3"
 - Reduces variability



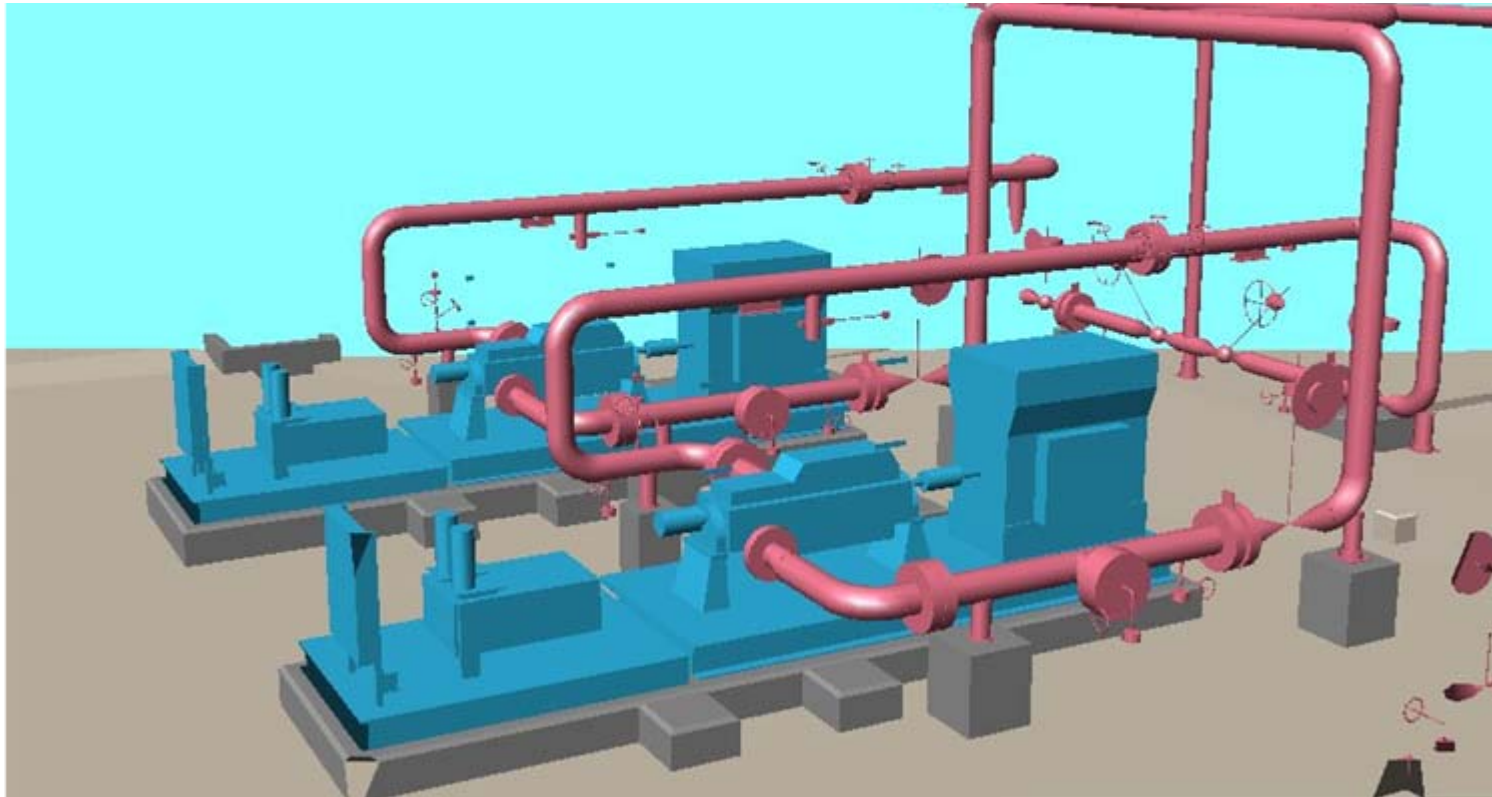
Special Piping Supports continued...

- Strut
 - Used for restraint of piping systems near critical equipment
 - Adjustable; zero gap, zero friction
 - Better than Guides and DAs at restraining thermal/friction loads
 - Not dependant on steel location; can adjust location inches at a time
- Teflon Slide Plate (TSP)
 - Reduces friction so support can slide easily
 - Usually placed under a shoe or base support
 - Allows expansion of pipe & equipment to reach steady state without overcoming a large friction force



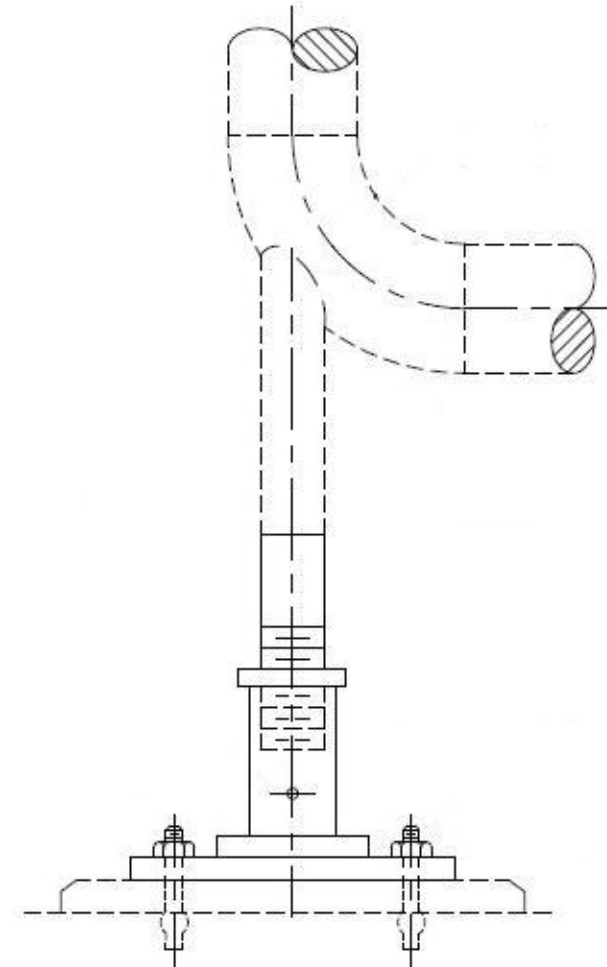
Typical Piping Layout

- Try to negate forces and moments by supporting the pipe at the same level as the pump. (Equal thermal growth)



Typical Piping Layout continued...

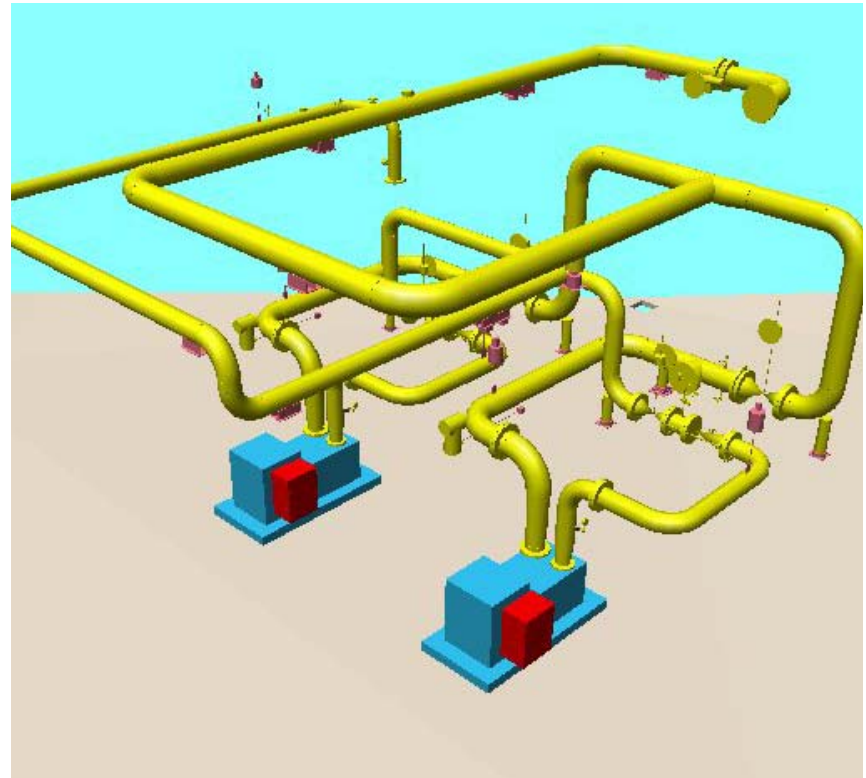
- First piping support before or after a nozzle is always an adjustable base support or a spring
 - Allows for proper alignment at site, as site conditions never match the elevations in model.
 - Example shown is mounted on an elbow, but these types of supports are used on straight runs of pipe as well.

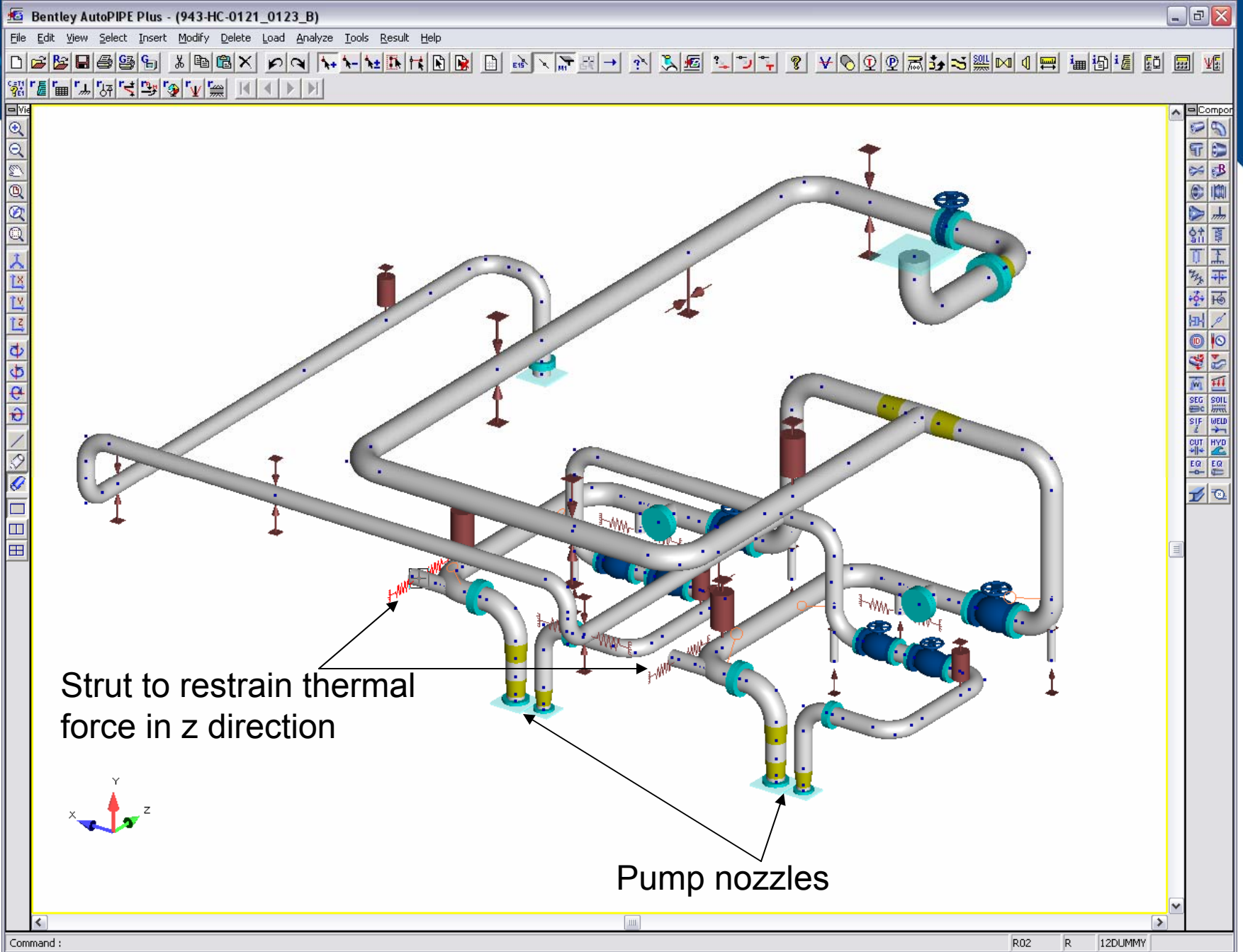


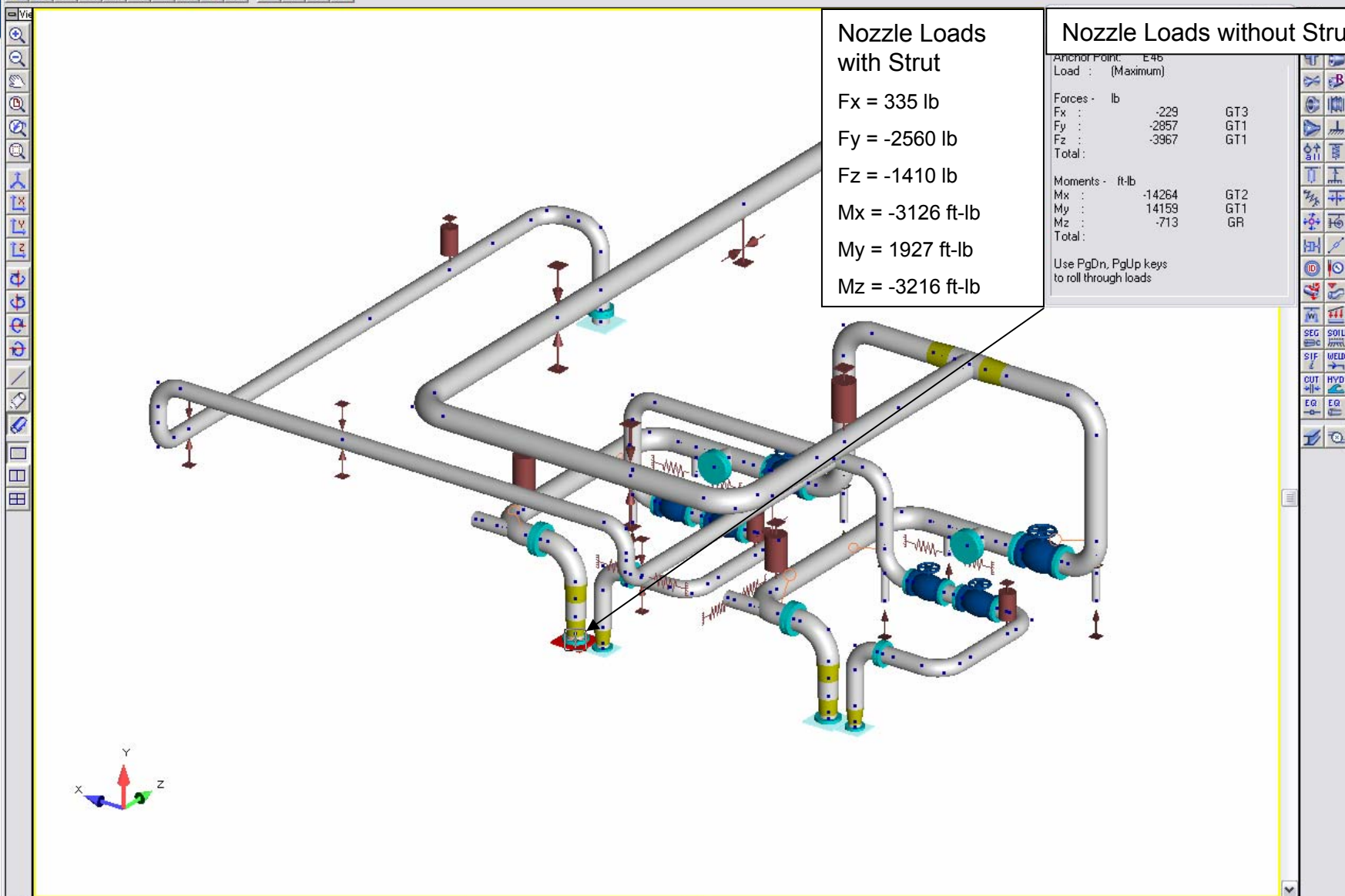
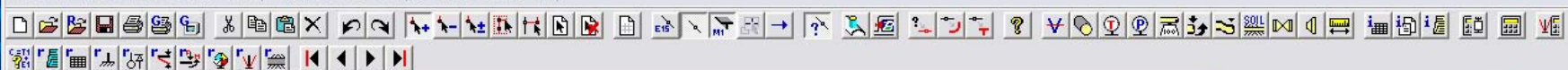
Typical Adjustable Base Support

Typical Piping Layout and Support – 2x100% Pumps

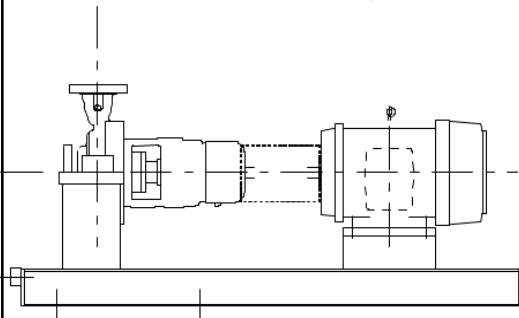
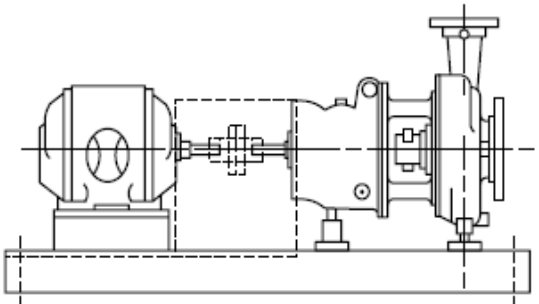
- Typical pump arrangements have one pump spared (i.e. not running)
- Thermal effect can be significant
- Piping layout is typically symmetrical for esthetics, and for equal flow if both pumps run together
- Minimize effect of downstream piping
- AutoPIPE® Break...
 - 14x10 BB2 Pumps
 - Flow = 4031gpm, Head = 241ft, HP = 300hp







API vs ANSI Pump Design

	API 610	ANSI B73.1
		
Mounting	Centreline	Foot
Casing Thickness Basis	Max discharge pressure	ASME B16.5 Class 150 flange P/T rating
Max Temperature	By Manufacturer	260°C
Flanges	Class 300	Class 150

API vs. ANSI Nozzle Loads

- All equipment codes have equations for nozzle loads
 - API 610 – Table 4 and Annex F
 - ANSI/HI 9.6.2
- API 610 allows us three options
 1. Individual Loads up to 1x Table 4 – OK
 2. Individual Loads up to 2x Table 4 – Apply Annex F
 - if all conditions of Annex F are met – OK
 3. Any individual load >2x Table 4 – Pump vendor must be informed to do a detailed analysis, or piping will have to change to reduce loads.

API vs. ANSI Nozzle Loads continued...

- Annex F allows us to normalize the forces and moments to take credit for low loads in a particular direction.
- Per API 610 5.5.5, “...use of Annex F methods can result in up to 50% greater misalignment than would occur using the loads of Table 4.”
- This risk is why the purchaser must agree to the use of Annex F.

API vs. ANSI Nozzle Loads continued...

Allowable Loads	API 610 Table 4		HI 9.6.2.1.1 Allowable Individual Nozzle Loads (ANSI Horizontal A80 6x4x13)	
	6" End Nozzle	4" Top Nozzle	6" End Nozzle	4" Top Nozzle
F_x (lb)	700	320	2700	1400
F_y (lb)	560	260	1350	1350
F_z (lb)	460	400	1500	3250
F_r (lb)	1010	570		
M_x (ft lb)	1700	980	1300	1200
M_y (ft lb)	870	500	1300	1500
M_z (ft lb)	1300	740	1100	690
M_r (ft lb)	2310	1330		

API vs. ANSI Nozzle Loads continued...

- ANSI nozzle loads don't look too bad when you look at the table on the previous slide
- Deceiving, because there are multiple tables, and a set of equations to meet, along with each table
- Depending on material, temperature and baseplate mounting, derating factors are applied to one or more of the tables, reducing the allowable loads.
- Recalling the first AutoPIPE® model...
 - 6x4 Horizontal Pump
 - Flow = 909gpm, Head = 426ft, HP = 150hp
- [API 610 Fluor Nozzle Load Spreadsheet...](#)
- [ANSI Fluor Nozzle Load Spreadsheet...](#)

API vs. ANSI Nozzle Loads continued...

- ANSI pumps are not built as robustly as API pumps and therefore have much lower allowable loads
 - At low temperatures ($<100^{\circ}\text{C}$), allowable nozzle loads can be met
 - ANSI pumps typically used for chemical or water services
 - REMEMBER TO CONSIDER MORE THAN INDIVIDUAL NOZZLE LOADS
- The Tradeoff
 - At higher temperatures, we have savings on the cost of the pump, but piping costs increase because of complex layouts and supports required to decrease the nozzle loads.
 - The economics of both the pump and piping (whole system) must be considered when choosing the pump.

Nozzle Load Issues for Different Pump Types

- Horizontal Overhung (OH2)
 - Stress engineers calculate the thermal growth of each nozzle and insert that into the assumed anchor of the AutoPIPE calculation.
- Vertical In-Line (OH3)
 - Stress engineering needs to know if these pumps are floating on the foundation.
 - If they are floating, the pump will move with the pipe expansion at startup to a steady state position.

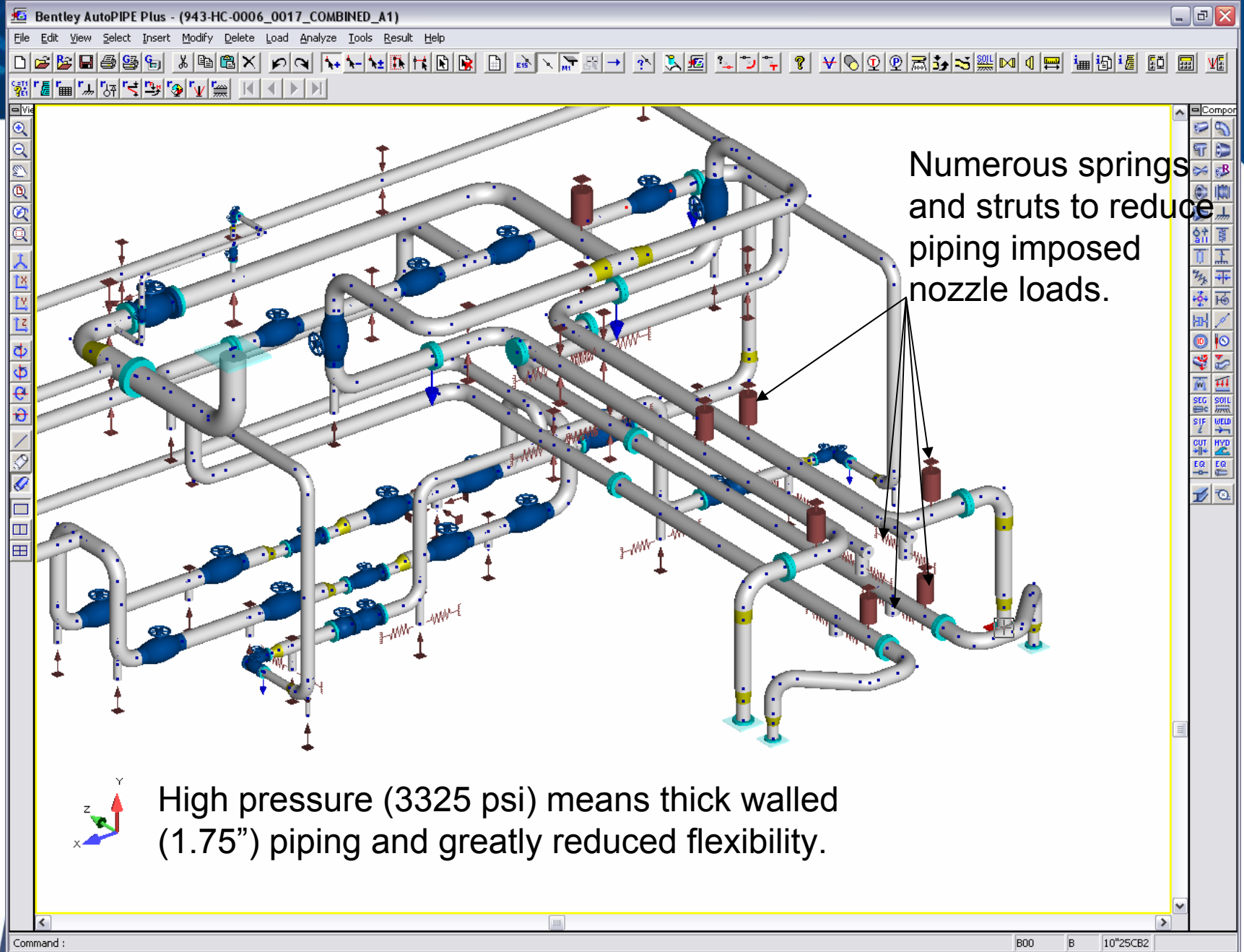
Nozzle Load Issues for Different Pump Types continued...

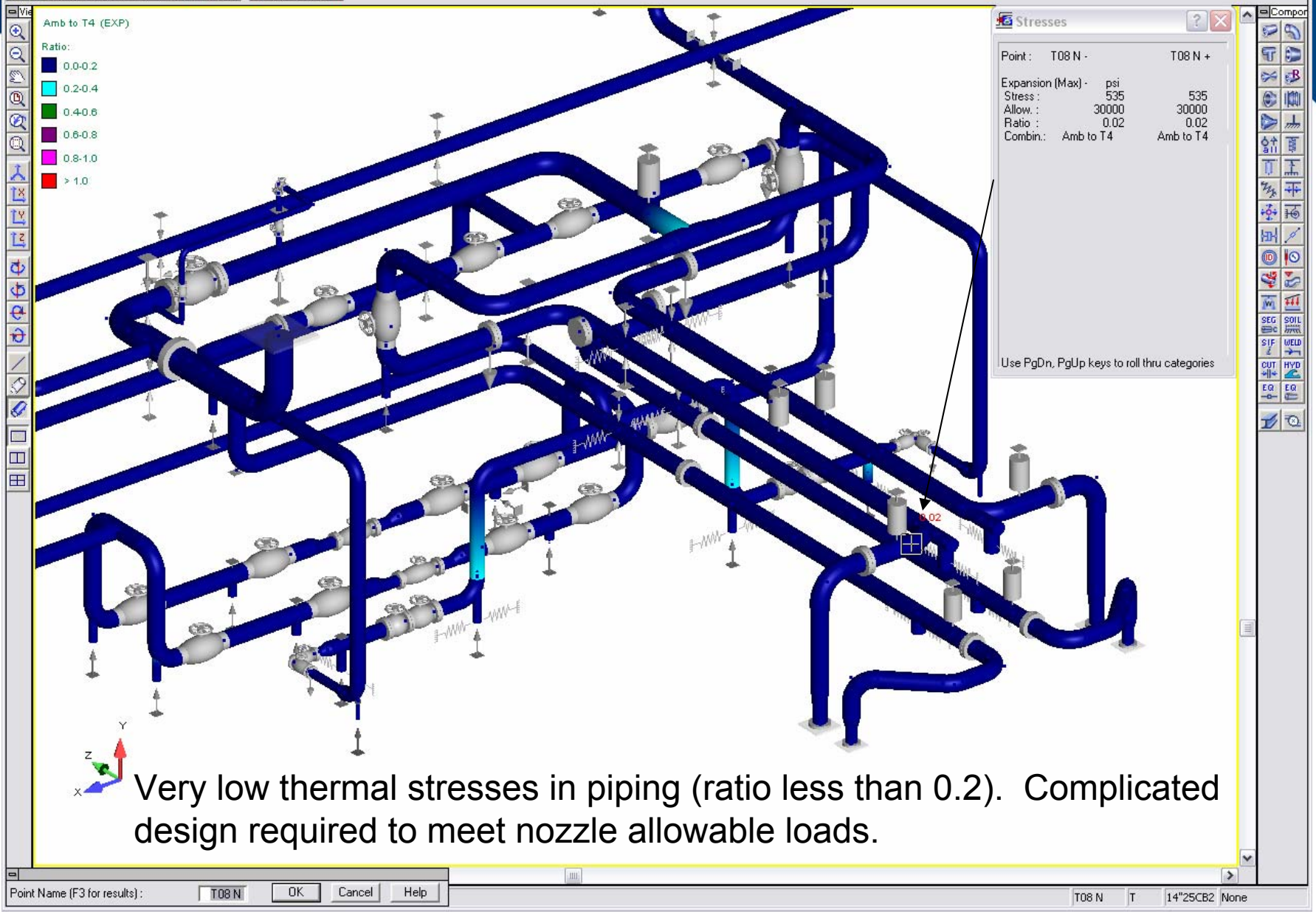
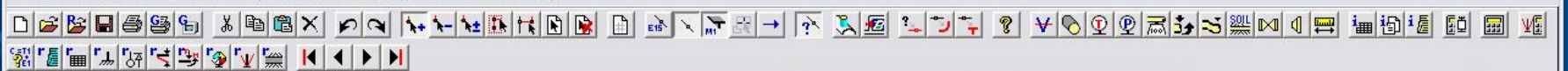
- Between Bearing (BB1, BB2, BB3, BB5)
 - Since these pumps are typically a top-top or side-side arrangement, the thermal growth of the nozzles is generally more significant.
 - Mechanical/Vendor needs to provide these values as piping can't always tell where the point of zero expansion is
 - This is especially true of a high-temperature (>200°C) barrel pump (BB5).

High Temperature Barrel Pump



- Nozzle Loads...
- AutoPIPE® Break...
 - 10x8 BB5 Pump
 - Flow = 1737gpm, Head = 6449, HP = 4500hp





Why is piping always bugging me?

- Piping needs the following information to do their work:
 - Pump type (API/ANSI)
 - GA Drawing of pump showing support location, nozzle distance from centreline, **vendor allowable loads**
 - Temperature info (usually from line list and P&ID)
 - Material of the pump (usually on the GA and datasheet)
 - ANSI flange size (150#, 300#, etc - usually on the GA or detailed drawings)
 - Nozzle movements from equipment zero point (point of zero thermal growth)
 - especially important for high temperature equipment
- This information is used for both the 3D model and the AutoPIPE® model.

Why is piping always bugging me?

Continued...

- Similar information is required for other types of equipment
- Complicated equipment like centrifugal compressors, heaters and reactors require more information from vendors like growth calculations, skin temperatures and layout of piping within the equipment
- Reciprocating compressors often require acoustic analysis to see how the vibrations of the equipment affect the piping
 - See API 618 (Section 7.9.4.2 and Annex N)
 - Analysis usually done by a third-party, and includes all piping and equipment
 - Also helps determine the need for pulsation suppression devices

Why is piping always bugging me?

Continued...

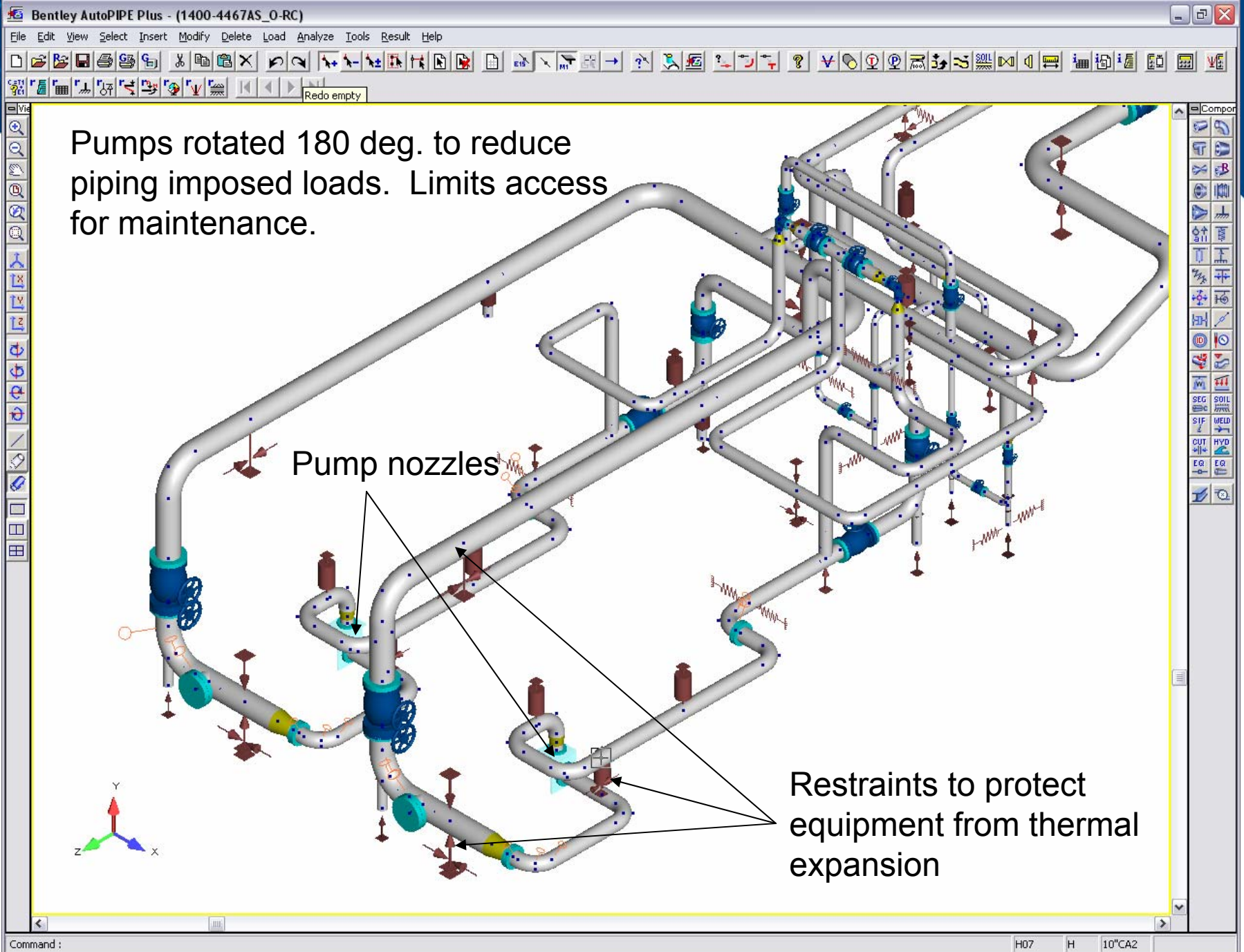
- Something to keep in mind:
 - **Mechanical data supports piping design**
 - Timely receipt of mechanical data is necessary to keep projects moving

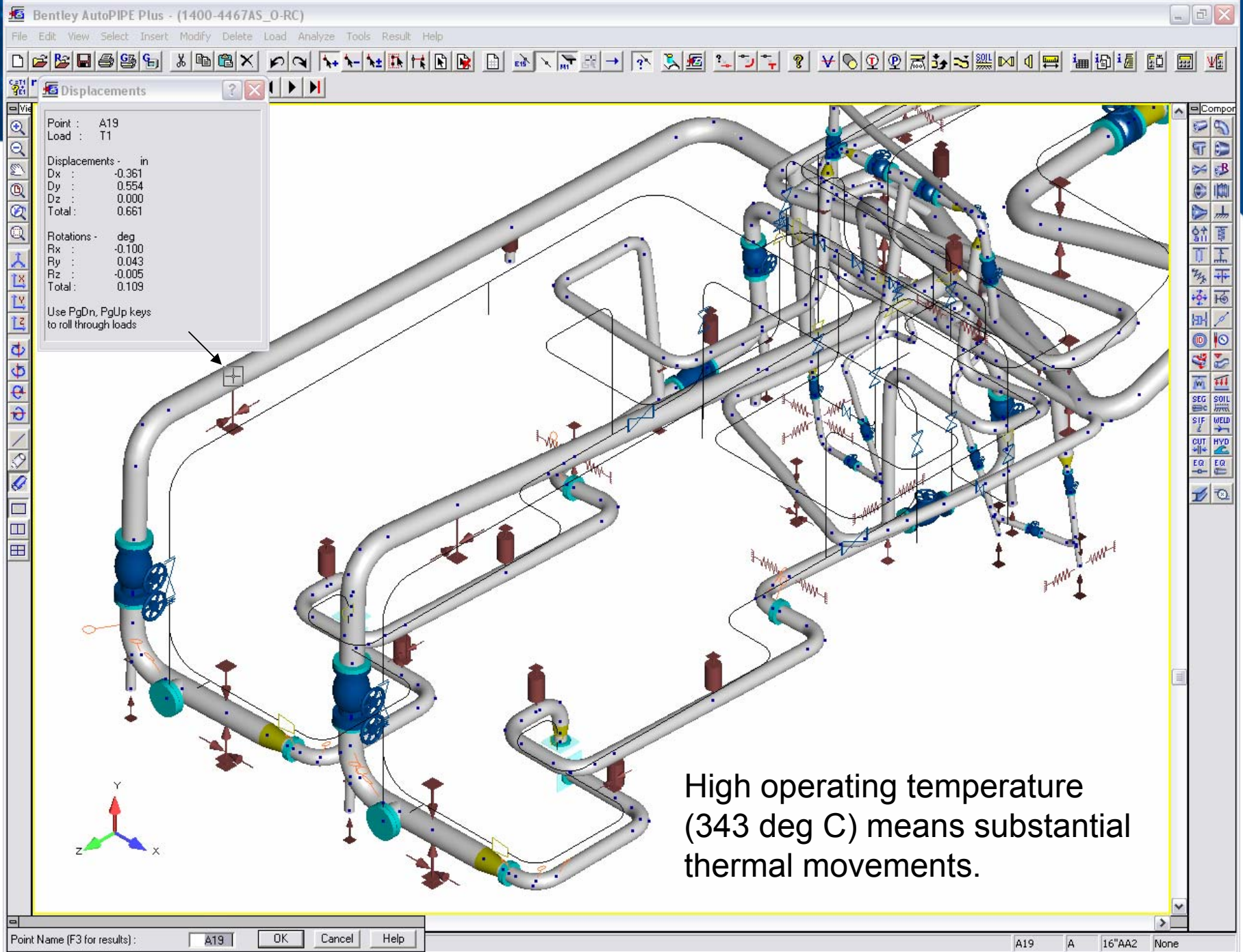
How can Nozzle Loads be Reduced?

- Increase piping flexibility (add loops)
- Add springs, struts and slide plates
- Add hot by-pass (very common)
- Can mount pumps on slide plates or springs
- In extreme cases, add expansion joints
 - Must be a low pressure system
 - Not recommended; expansion joint is usually the weakest point in the system

Examples of Special Cases

- Heavy Flanges (ANSI 1500#)
 - See Barrel Pump Example
- High Temperature Pumps
 - See Barrel Pump Example
- Sea Water Pumps (HDPE piping)
 - Expansion joints
- Reciprocating Compressors
 - Cast cylinder heads; very low allowable loads
 - Hold down supports, snubbers
- Steam Turbines
- Screw Pump Example...
 - 10x8 Screw Pump
 - Flow = 198.95 m³/h, ΔP = 2255 kPa, HP = 300hp





References

- Pumps
 - API 610 10th Ed., Section 5.5 and Annex F
 - ANSI/HI 9.6.2 – Centrifugal and Vertical Pumps for Allowable Nozzle Loads
 - PIP RESP002 – Design Of ASME B73.1 And General Purpose Pump Baseplates
- Compressors
 - API 617 7th Ed., Section 2.3.4 and Annex 2.E
 - API 618 5th Ed., Section 7.9.4.2 and Annex N
 - API 619 4th Ed., Section 5.4 and Annex C
- Piping
 - ASME B31.3 – 2008, Chapter II Part 5 – Flexibility and Support

Thank you!



Any questions?

Feel free to contact us:

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