Sections 10.2 and 3

Purchasing Guidelines and Design Requirements

10.2

Purchasing Guidelines

This appendix provides recommended guidelines for inquiry and purchase of API Choke and Kill Systems Equipment. The purchaser should provide rated working pressure, temperature ratings and size designation, when placing an order or making an inquiry.

10.2.1

Size Designation

The size designation consists of the nominal through bore dimension. A list of standard sizes is found in Section 3 of this specification.

10.2.2 Rated Wor

Rated Working Pressure

The rated working pressure is determined by the lowest rated working pressure of the component or assembly, including integral end or outlet connections. Standard rated working pressures are listed in Section 3.

10.2.3

Temperature Rating

The minimum temperature rating is based on the lowest ambient temperature to which the equipment may be subjected during operation. The maximum temperature rating is the highest temperature of the fluid which may flow through the equipment.

10.2.3.1 Metallic Materials

Metallic equipment should be designed to operate in one of the temperature ratings listed in Section 3.

10.2.3.2 Non-Metallic Materials

Non-metallic equipment and components, including seals, should be designed to operate in one of the temperature ranges listed in Section 3.

Section 3 Design Requirements

3.1

Design Method

Design method shall be in accordance with one or more of the following criteria.

3.1.1

ASME Method

The design methodology as described in the ASME Boiler and Pressure Vessel Code, Section VIII, Division 2, Appendix 4, shall

(Continued to next column)

be used for design calculations. Design allowable stresses shall be limited by the following criteria:

$S_m = 2/3 S_v \text{ and } S_t = 0.9 S_v$

where

- S_m = design stress intensity at rated working pressure
- S_v = material minimum specified yield strength
- St = maximum allowable primary membrane stress intensity at hydrostatic test pressure.

3.1.2

Distortion Energy Theory Method

The Distortion Energy method shall be used for design calculations for unions. The minimum pressure design thickness shall be calculated by combining triaxial stresses based on the distortion energy method, using either one of the limits below. Secondary stresses and stress concentrations are beyond the scope of this method.

1. The rated working pressure

 $S_{e} = 2/3 S_{v}$

 S_e = von Mises equivalent stress

2. The hydrostatic test pressure limited by the following criterion:

 $S_e = S_y$

3.1.3

Experimental Stress Analysis

Experimental Stress Analysis as described in ASME Boiler and Pressure Vessel Code, Section VIII, Division 2, Appendix 6, shall be used.

3.1.4

Proof Test Analysis

Proof testing as described in ASME Boiler and Pressure Vessel Code, Section VIII, Division 1, Part UG-101, shall be used.

3.2

Performance Requirements

Performance requirements are specific and unique to the product in the as-shipped condition. Products shall be designed to perform according to the requirements of this section and in the pressure, temperature ranges, test fluids, and in accordance with Section 4.

Handbook Revision 10.01.09

Refer to pages 50 and 14 - 16 of API Spec 16C Purchase API Spec 16C online at www.global.ihs.com

Sections 10.2 and 3 **Purchasing Guidelines and Design Requirements**

321

3.2.1	Table 3.4.1 – Equipment Bore Sizes and Rated Working Pressure			
Pressure Integrity Products shall be capable of withstanding rated working pressure at rated temperature without deformation to the extent that any other performance requirement is not met.	Size (minimum through bore) in. (mm)	Rated Working Pressure psi (MPa)		
3.2.2	2 1/16 (52)	2000 (13.8)		
Thermal Integrity	2 ⁹ / ₁₆ (65)			
Products and/or systems shall be capable of functioning throughout the temperature range of which they are rated.	3 ½ (78)			
222	4 ½ (103)			
5.2.5 Leakage				
No visible leakage is allowed.	2 1/16 (52)	3000 (20.7)		
324	2 % (65)			
Load Capability	3 ½ (78)			
Products shall be capable of sustaining rated loads without deformation to the extent that any other performance	4 ½ ₆ (103)			
requirement is not met.	2 1/16 (52)	5000 (34.5)		
3.2.5	2 % (65)			
Cycles Products shall be capable of performing and operating as	3 ½ (78)			
9 for applicable products.	4 ½ (103)			
3.2.6	1 13/16 (46)	10,000 (69.0)		
Operating Force or Torque	2 1/16 (52)			
the manufacturer's written specification, which includes	2 % (65)			
acceptance criteria.	3 1/16 (78)			
3.3	4 ½ (103)			
Performance Verification				
of new products and on designs resulting from changes.	1 11/16 (46)	15,000 (103.5)		
Verification testing specified in this section is intended to be	2 1/16 (52)			
performed on line samples representative of production models.	2 % (65)			
3.3.1	3 1/16 (78)			
Performance Verification Requirements Performance verification requirements are set forth in Section 9.	4 ½ ₁₆ (103)			
3.3.2	1 13/16 (46)	20,000 (138)		
Product Changes	2 1/16 (52)			
design requiring performance verification. A substantive change	2 % (65)			
is a change identified by the manufacturer which affects the	3 ¼ (78)			
This includes changes in fit, form, function or material.	4 ¼ (103)			

3.4

Bore sizes and Rated Working Pressure

The bore size and rated working pressure designation of a choke and kill system and the components shall consist of the values delineated in Table 3.4.1, Equipment Bore Sizes and Rated Working Pressure, Table 3.4.2 and Table 3.4.3.

Note: Specific size and pressure rating combinations are not necessarily available for each type of end or outlet connection (e.g., flange, hub and threaded).

Sections 10.2 and 3 Purchasing Guidelines and Design Requirements

Table 3.4.2 – Union, Swivel Joint and Articulated Line Sizes and

 Rated Working Pressures

 Table 3.4.3 - Flexible Line Sizes and Rated Working Pressures

Nominal Size in. (mm)	Rated Working Pressure psi (MPa)	ID in. (mm)	Rated Working Pressure psi (MPa)
2 (50.8)	3,000 (20.7)	2 (50.8)	5,000 (34.5)
3 (76.2)		3 (76.2)	
4 (101.6)		3 ½ (88.9)	
1 (25.4)	5,000 (34.5)	4 (101.6)	
1 ½ (38.1)		2 (50.8)	10.000 (69.0)
2 (50.8)		2 ½ (63.5)	
3 (76.2)		3 (76.2)	
4 (101.6)		4 (101.6)	
1 (25.4)	10,000 (69.0)	2 (50.8)	15,000 (103.5)
2 (50.8)		2 ½ (63.5)	
3 (76.2)		3 (76.2)	
4 (101.6)	-	· · · ·	
2 (50.8)	15.000 (103.5)	2 (50.8)	20,000 (138)
2 ½ (63.5)		2 ½(63.5)	
3 (76.2)		3 (76.2)	
	-		
2 (50.8)	20,000 (138)		
2 ½ (63.5)			
3 (76.2)			

3.5 Service

Service Conditions

3.5.1

Rated Working Pressure

Equipment within the scope of this specification shall be rated in only the following working pressures, psi (MPa): 2000 (13.8), 3000 (20.7), 5000 (34.5), 10,000 (69.0), 15,000 (103.5), and 20,000 (138.0) psi (MPa), as delineated in Section 3.4.

3.5.2

Temperature Ratings

Minimum temperature is the lowest ambient temperature to which the equipment may be subjected, while in service. Maximum temperature is the highest fluid temperature which may flow through the equipment, while in service. Equipment shall be designed to operate within the temperature ranges shown in Table 3.5.2.1.

 Table 3.5.2.1 – Temperature Rating for Metallic and Nonmetallic

 Materials and Flexible Lines

Rating	Operating Range °F (°C)	
А	-4 to 180	(-20 to 82)
В	-4 to 212	(-20 to 100)
К	-75 to 180	(-60 to 82)
Р	-20 to 180	(-29 to 82)
U	0 to 250	(-18 to 121)

3.5.3

Fluid Service Conditions

Choke and Kill Systems are generally mobile and may be expected to be used in areas wher sour service conditions may be encountered. Metallic materials which come in contact with the well fluid shall meet the requirements of NACE Standard MR0175-91.

3.5.4

Flange and Hub End and Outlet Connections

Flanges and hubs are designed in accordance with design criteria and methods developed by the API Committee on Standardization of Valves and Well-head Equipment and the API Committee for Drill-Through Equipment. End and outlet connections are described in this specification. Design is not within the scope of this specification. Manufacturers shall make the end and outlet connections as per the applicable sections of API Specifications 6A and 16A.

Sections 10.2 and 3 Purchasing Guidelines and Design Requirements

3.6 Closure Bolting

The maximum allowable tensile stress for closure bolting shall be determined considering initial bolt up rated working pressure, and hydrostatic test pressure conditions. Bolting stresses, based on the root area of the thread, shall not exceed the following limits:

 $S_{a} = 0.83S_{v}$

where

S_a = maximum allowable tensile stress

 S_v = bolting material specified minimum yield strength

Bolting Stresses shall be determined considering all loading on the closure including pressure acting over the seal area, gasket loads and any additive mechanical and thermal loads.

3.7

Clamps

Clamps for API 16BX Hubs are not included in this specification edition or the current API Spec 16A. Clamps will be addressed in a future edition of these specifications.

3.9

Test, Vent, Pipe Plugs and Gauge Connections

Test, Vent, Pipe Plugs and Gauge Connections for use on 2000 (13.8), 3000 (20.7), 5000 (34.5), 10,000 (69.0), 15,000 (103.5), and 20,000 (138.0) psi (MPa) equipment shall be as per API Spec 6A, Section 911. Vent connections shall be in accordance with manufacturers written specifications.

3.10

Design Documentation

Documentation of designs shall include methods, assumptions, calculations, and design requirements. Design documentation media shall be clear, legible, reproducible and retrievable.

3.10.1

Design Review

Design documentation shall be reviewed and verified by qualified personnel other then those who created the original design.

3.10.2

Design Verification

Manufacturer's shall document their verification procedures and the results of performance verification of designs. Design verification is not required on API flanges, hubs and ring gaskets.

3.10.3

Documentation Retention

Design documentation shall be retained for ten years after the last unit of that model, size and rated working pressure is manufactured.

Handbook Revision 10.01.09

Refer to pages 50 and 14 - 16 of API Spec 16C Purchase API Spec 16C online at www.global.ihs.com

Sections 10.2 and 3 Purchasing Guidelines and Design Requirements

Table 3.8 - Fraction to Decimal Conversion

Table 3.8 - Fraction to Decimal Conversion (continued)

	8th	16th	32nd	64th	0.000	0.00
			•	1/64	0.016	0.02
			1/32		0.031	0.03
				3/64	0.047	0.05
		1/16		,	0.062	0.06
		L ,		5/64	0.078	0.08
			3/32		0.094	0.09
				7/64	0.109	0.11
	1/8				0.125	0.12
ı				9/64	0.141	0.14
			5/32		0.156	0.16
				11/64	0.172	0.17
		3/16		·	0.188	0.19
		<u> </u>		13/64	0.203	0.20
			7/32	·	0.219	0.22
				15/64	0.234	0.23
1/	4				0.250	0.25
				17/64	0.266	0.27
			9/32		0.281	0.28
				19/64	0.297	0.30
		5/16			0.312	0.31
				21/64	0.328	0.33
			11/32		0.344	0.34
				23/64	0.359	0.36
	3/8				0.375	0.38
				25/64	0.391	0.39
			13/32		0.406	0.41
				27/64	0.422	0.42
		7/16			0.438	0.44
				29/64	0.453	0.45
			15/32		0.469	0.47
				31/64	0.484	0.48
1/	2				0.500	0.50

-	Oth	4 0+1-	2011	0.444	0.000	0.00
	Sth	16th	32nd	64th	0.000	0.00
				33/64	0.516	0.52
			17/32		0.531	0.53
				35/64	0.547	0.55
		9/16			0.562	0.56
				37/64	0.578	0.58
			19/32		0.594	0.59
				39/64	0.609	0.61
	5/8				0.625	0.62
				41/64	0.641	0.64
			21/32		0.656	0.66
				43/64	0.672	0.67
		11/16			0.688	0.69
				45/64	0.703	0.70
			23/32		0.719	0.72
				47/64	0.734	0.73
3/	4				0.750	0.75
				49/64	0.766	0.77
			25/32		0.781	0.78
				51/64	0.797	0.80
		13/16			0.812	0.81
				53/64	0.828	0.83
			27/32		0.844	0.84
				55/64	0.859	0.86
	7/8				0.875	0.88
				57/64	0.891	0.89
			29/32		0.906	0.91
				59/64	0.922	0.92
		15/16			0.938	0.94
				61/64	0.953	0.95
			31/32		0.969	0.97
				63/64	0.984	0.98
1					1.000	0.100

(Continued to next column)