



LEGENDS
Calgary, Alberta
CANADA

Case Name: C:\Documents and Settings\Owner\Desktop\PIPESYS\uk_2.hsc
Unit Set: SI
Date/Time: Mon Oct 16 15:59:25 2017

NeotecPIPESYS v2.01:

uk_2.hsc

op-100

Cooldown

Results

Cumulative Length (m)	Overall Heat Transfer Coefficient (kJ/h-m ² -C)	Inside Film Coefficient (kJ/h-m ² -C)	Fluid Thermal Conductivity (W/m-K)	First Intermediate Temperature (C)	Second Intermediate Temperature (C)	Third Intermediate Temperature (C)	Temperature for Max Time Since Shutdown (C)	Time to Reach Min Cooldown Temperature (hours)

Inlet Properties : inlet

	Overall	Vapour Phase		
Vapour/Phase Fraction	1.0000	1.0000		
Temperature: (C)	45.00 *	45.00		
Pressure: (kPa)	8000.00 *	8000.00		
Molar Flow (kgmole/h)	300.00 *	300.00		
Mass Flow (kg/h)	5512.61	5512.61		
Liquid Volume Flow (m ³ /h)	16.82	16.82		
Std Gas Flow (STD_m ³ /h)	7093.33	7093.33		
Molar Enthalpy (kJ/kgmole)	-8.188e+004	-8.188e+004		
Mass Enthalpy (kJ/kg)	-4456	-4456		
Heat Flow (kJ/h)	-2.457e+007	-2.457e+007		
Molar Density (kgmole/m ³)	3.4253	3.4253		
Mass Density (kg/m ³)	62.942	62.942		
Std Liquid Mass Density (kg/m ³)	---	---		
Molar Heat Capacity (kJ/kgmole-C)	49.646	49.646		
Mass Heat Capacity (kJ/kg-C)	2.702	2.702		
Molar Entropy (kJ/kgmole-C)	149.938	149.938		
Mass Entropy (kJ/kg-C)	8.160	8.160		
ThermalConductivity (W/m-K)	0.042	0.042		
Viscosity (cP)	0.014	0.014		
Surface Tension (dyne/cm)	---	---		
Molecular Weight	18.375	18.375		
Z Factor	0.883	0.883		

Outlet Properties : out

	Overall	Vapour Phase		
Vapour/Phase Fraction	1.0000	1.0000		
Temperature: (C)	27.01	27.01		
Pressure: (kPa)	7692.76	7692.76		
Molar Flow (kgmole/h)	300.00 *	300.00		
Mass Flow (kg/h)	5512.61	5512.61		
Liquid Volume Flow (m ³ /h)	16.82	16.82		
Std Gas Flow (STD_m ³ /h)	7093.33	7093.33		
Molar Enthalpy (kJ/kgmole)	-8.273e+004	-8.273e+004		
Mass Enthalpy (kJ/kg)	-4502	-4502		
Heat Flow (kJ/h)	-2.482e+007	-2.482e+007		
Molar Density (kgmole/m ³)	3.6161	3.6161		



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Outlet Properties : out

		Overall	Vapour Phase		
16	Mass Density (kg/m3)	66.447	66.447		
17	Std Liquid Mass Density (kg/m3)	---	---		
18	Molar Heat Capacity (kJ/kgmole-C)	51.131	51.131		
19	Mass Heat Capacity	2.783	2.783		
20	Molar Entropy (kJ/kgmole-C)	147.484	147.484		
21	Mass Entropy (kJ/kg-C)	8.026	8.026		
22	Thermal Conductivity (W/m-K)	0.040	0.040		
23	Viscosity (cP)	0.014	0.014		
24	Surface Tension (dyne/cm)	---	---		
25	Molecular Weight	18.375	18.375		
26	Z Factor	0.852	0.852		

Stream Compositions

Component	Inlet Mole Fraction	Outlet Mole Fraction
31 Methane	0.89592 *	0.89592 *
32 Ethane	0.04907 *	0.04907 *
33 i-Butane	0.00243 *	0.00243 *
34 n-Butane	0.00778 *	0.00778 *
35 CO2	0.01708 *	0.01708 *
36 H2S	0.00523 *	0.00523 *
37 i-Pentane	0.00188 *	0.00188 *
38 n-Pentane	0.00183 *	0.00183 *
39 n-Hexane	0.00026 *	0.00026 *
40 Propane	0.01208 *	0.01208 *
41 Nitrogen	0.00643 *	0.00643 *



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Summary

Upstream Pressure: 8000.00 kPa
Upstream Temperature: 45.00 C

Downstream Pressure: 7692.76 kPa
Downstream Temperature: 27.01 C

Predicted Pressure Loss: 307.24 kPa

Friction Loss: 131.76 kPa
Hydrostatic Loss: 175.46 kPa
Kinetic Loss: 0.021 kPa

Inline Facilities Loss: 0.00 kPa

Average Pressure Gradient: -0.1020 kPa/m

Total Liquid Holdup: 0.0 m3
Total Line Pack @STD: 2072.5 m3

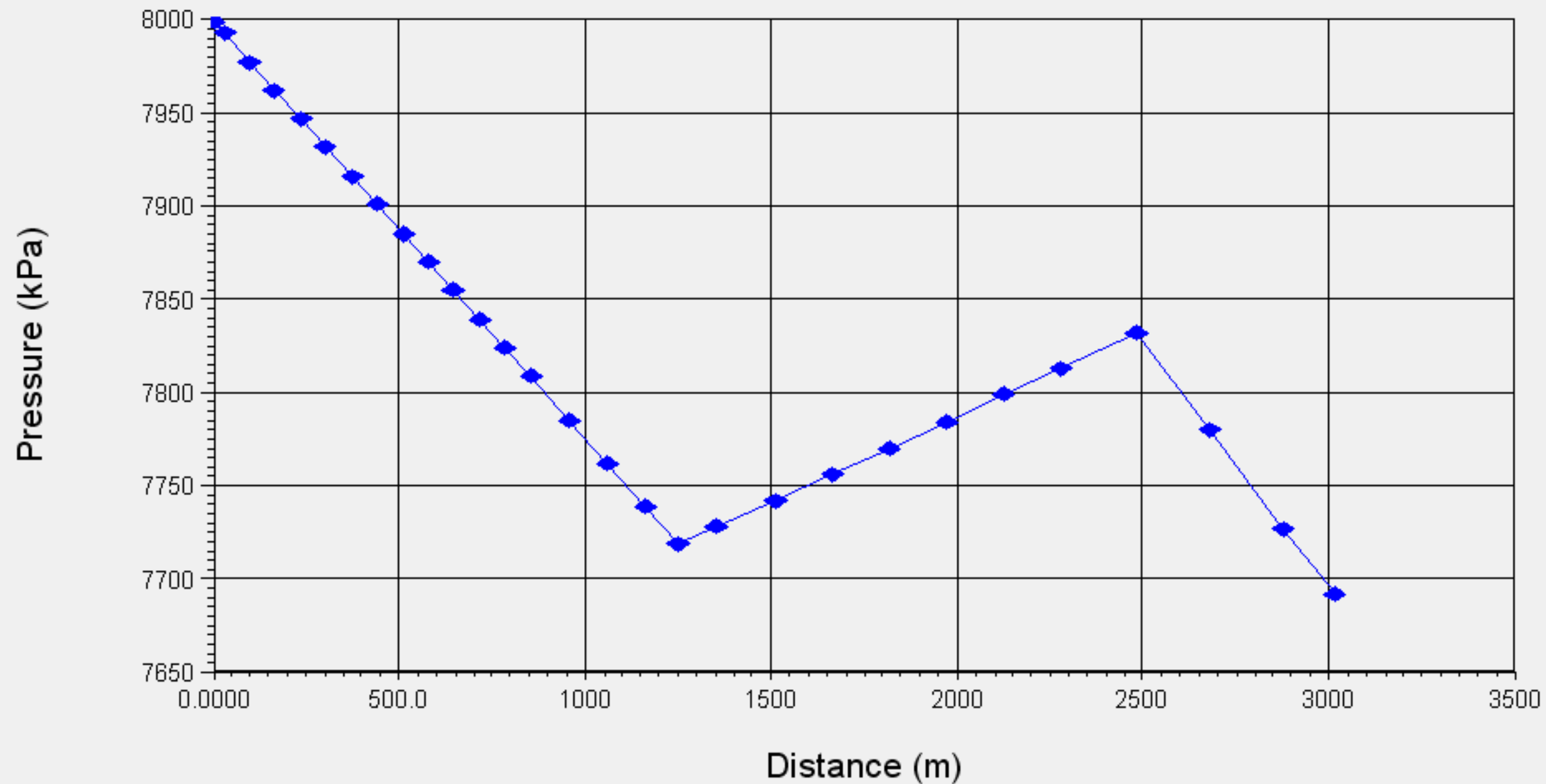
Pipe Volume: 24.7 m3

Net Heat Loss to the Surroundings: 2.383e+005 kJ/h

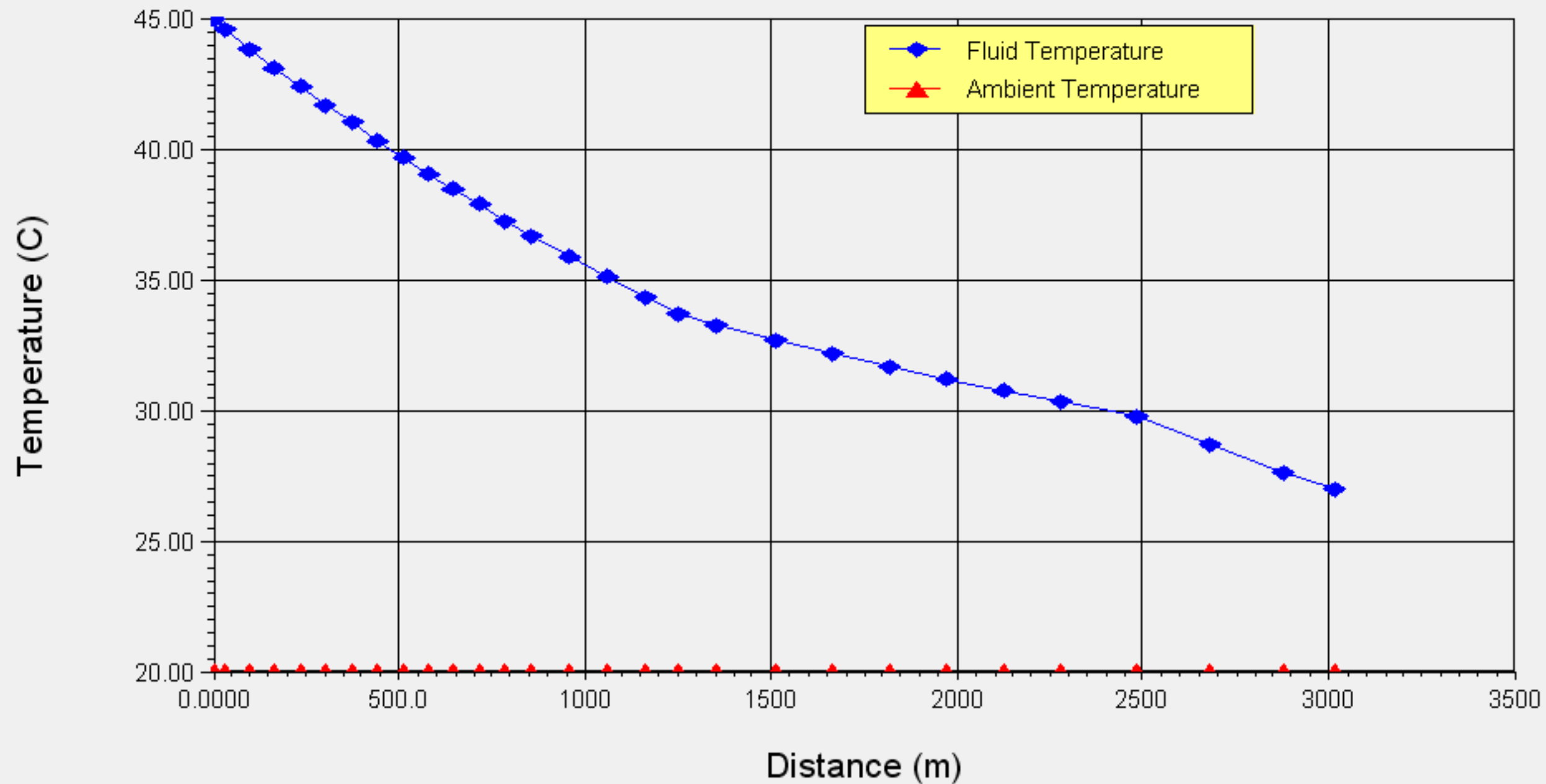
Pipeline Elevation: op-100



Flowing Pressure: op-100



Flowing Temperature: op-100



Actual Gas Velocity: op-100

